

Hydrogenation of biomass derived oxygenates to biochemicals

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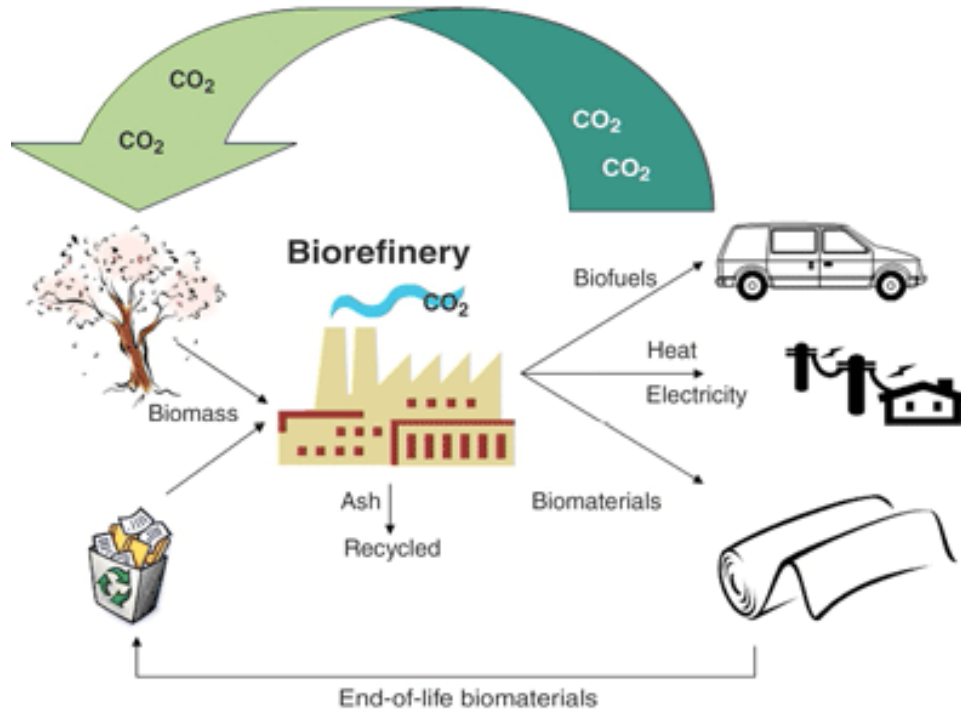
Esben Taarning, Haldor-Topsøe

Matthias Beier, Haldor-Topsøe

WP 2.4

The logo for BIO4 FUELS features the word "BIO" in green, followed by a large, stylized "4" in a lighter green shade, and the word "FUELS" in green below it.

Biorefinery concept



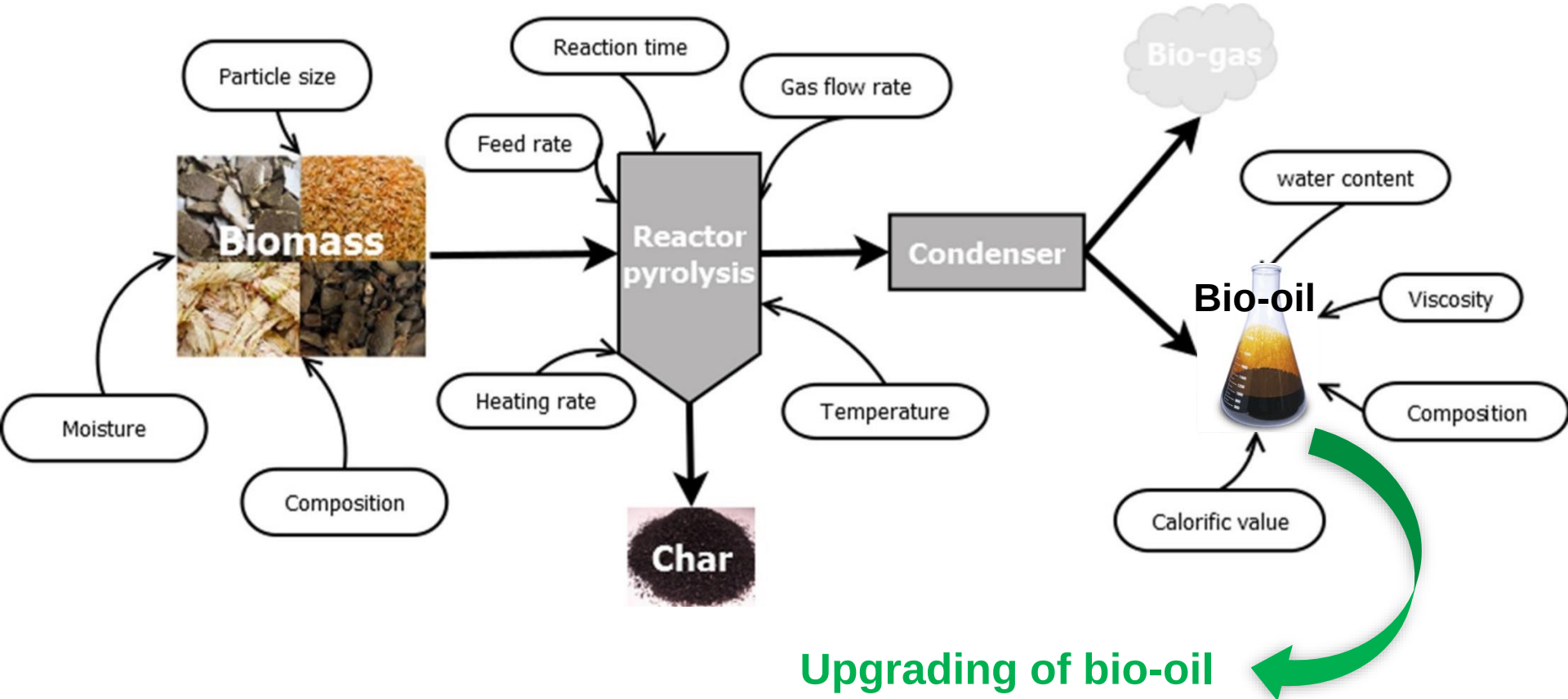
Integrated production

- Fuels
- Energy
- Chemicals
- Materials



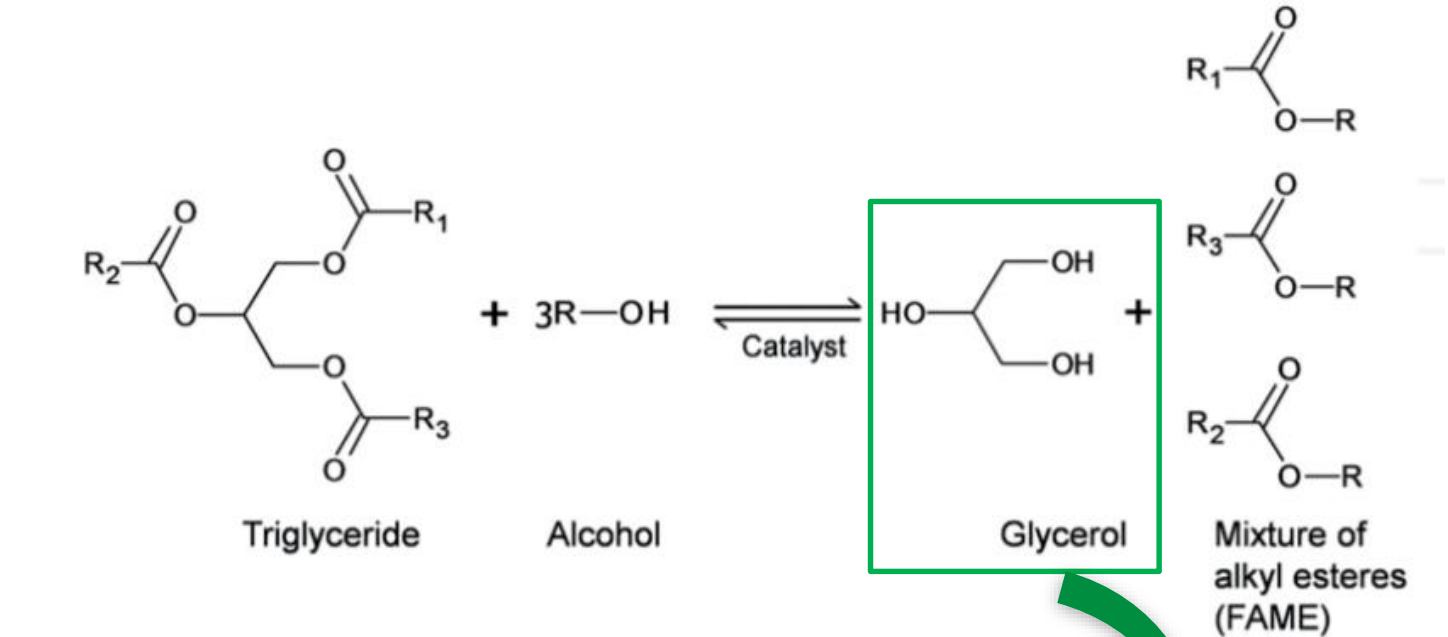
Increase
economic sustainability

Biomass pyrolysis



Upgrading of bio-oil

Transesterification of vegetable oil for biodiesel production



R_1, R_2, R_3 = Hydrocarbon chain ranging from 15 to 21 carbon atoms

Glycerol utilization

Sugars cracking

Sugars → Intermediates → biochemicals

- MEG (monoethylene glycol) via hydrogenation
- MVG (methyl vinyl glycolate) via retro-aldol chemistry



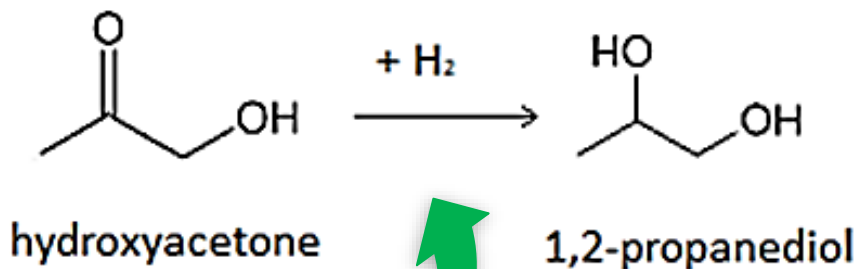
MOSAIK™
monosaccharide
industrial cracker



MOSAIK™ - From **sugars** to a range of **chemicals**,
commodities (MEG) to specialties (MVG)



Hydroxyacetone hydrogenation to 1,2-propanediol



Copper catalyst

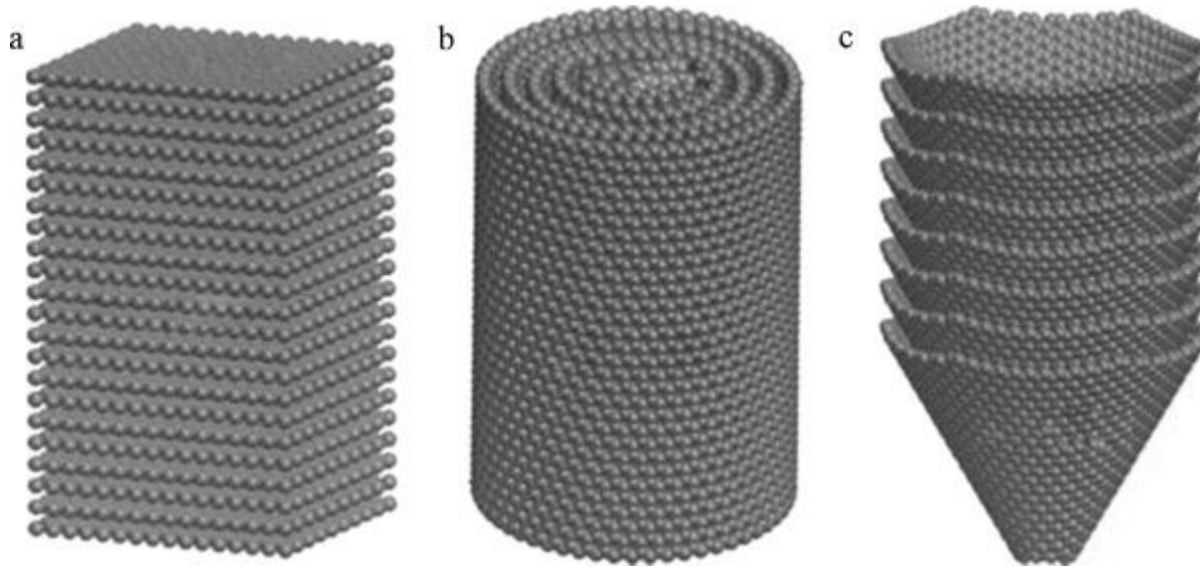
- ✓ Active
- ✓ Selective
- ✓ Stable

Catalyst preparation - 5wt% Cu

<i>support</i>	<i>precursor</i>	<i>solvent</i>
SiO ₂	Copper(II) nitrate Cu(NO ₃) ₂	H ₂ O
		EtOH
		iso-PrOH
	Copper(II) acetate Cu(CH ₃ COO) ₂	H ₂ O
		EtOH
		iso-PrOH
	Basic Copper(II) carbonate CuCO ₃ ·Cu(OH) ₂	H ₂ O
		EtOH
		iso-PrOH

Catalyst support

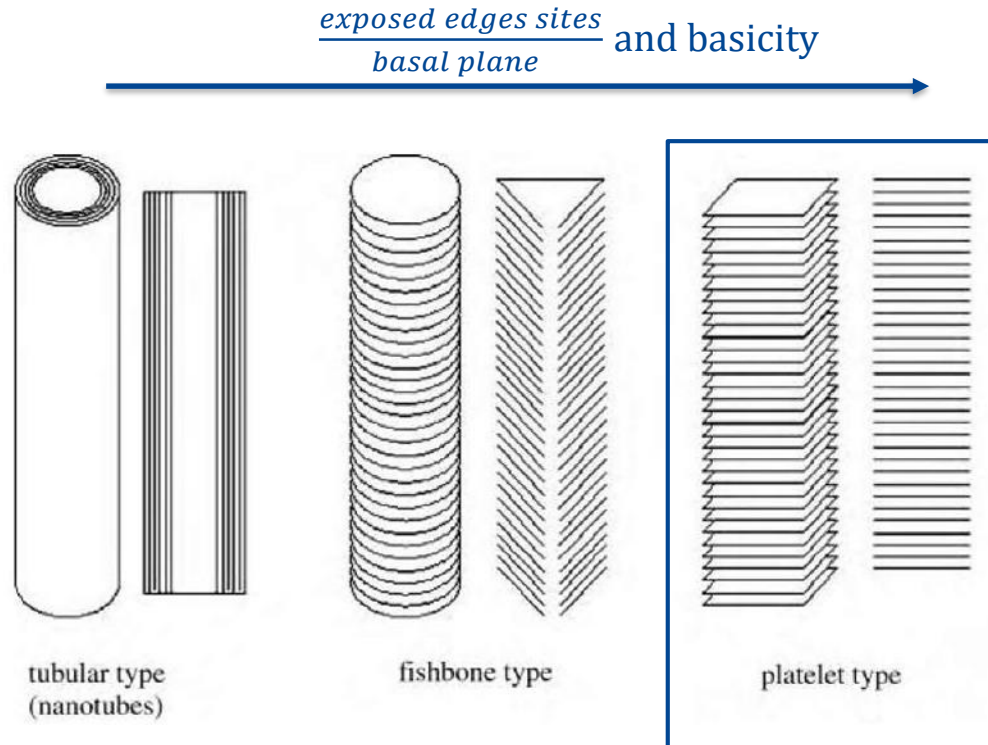
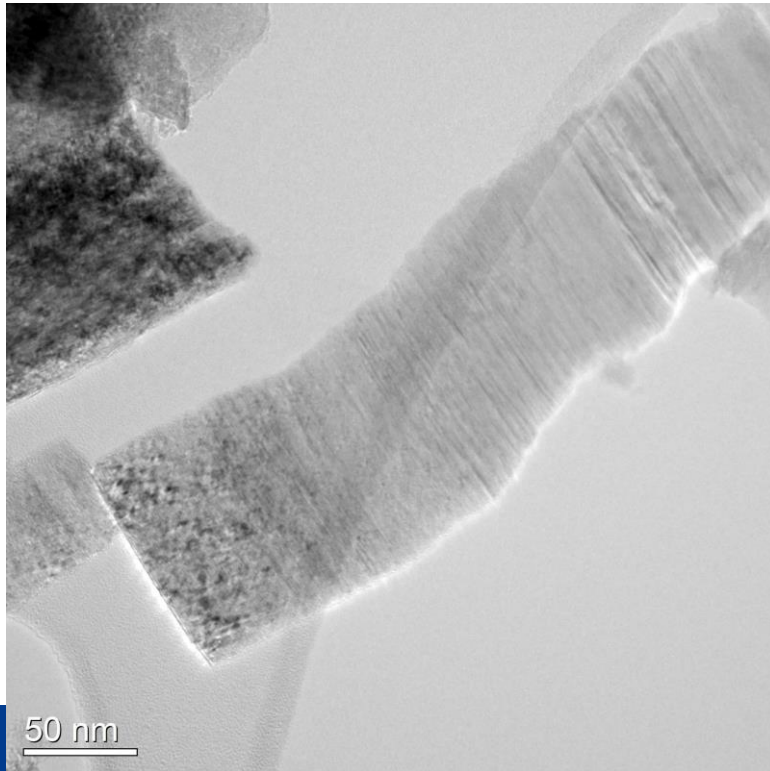
Carbon Nanofibers



- high surface area:
 $10\text{-}300\text{ m}^2/\text{g}$
- large number of edges:
anchoring sites for
catalyst precursors
- surface properties
adjusted by surface
oxidation and foreign-
ion doping

Catalyst support - *Carbon Nanofibers*

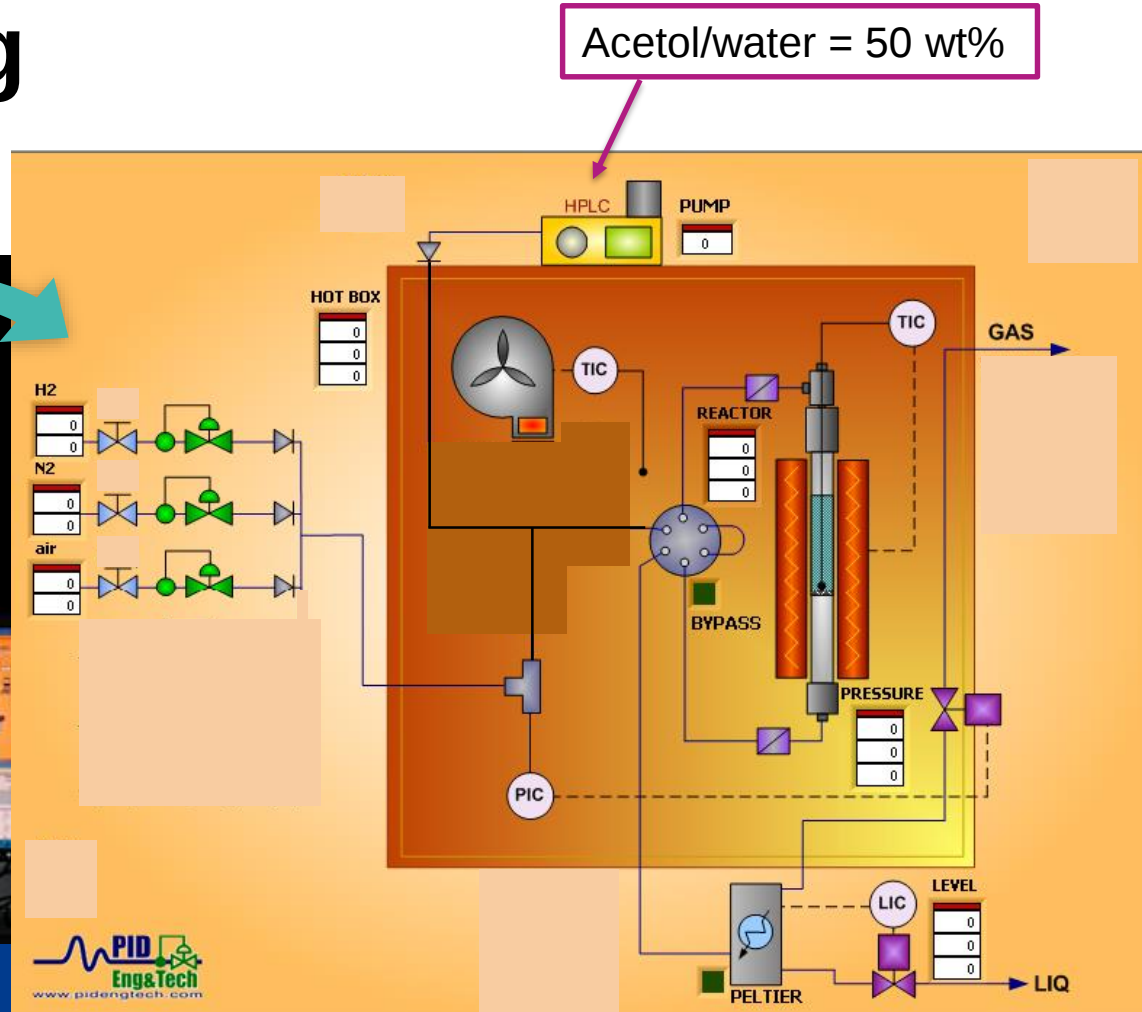
Platelet type



Catalyst preparation - 5wt%Cu

<i>support</i>	<i>precursor</i>	<i>solvent</i>	<i>CNF pretreatment</i>
PCNF	Copper(II) nitrate $\text{Cu}(\text{NO}_3)_2$	H_2O	/
		EtOH	/
		iso-PrOH	/
			HNO_3
			Ar @ 700°C
			HNO_3 Ar @ 700°C
			HNO_3 Ar @ 1000°C
	Basic Copper(II) carbonate $\text{CuCO}_3 \cdot \text{Cu}(\text{OH})_2$	H_2O	/
		EtOH	/
		iso-PrOH	/

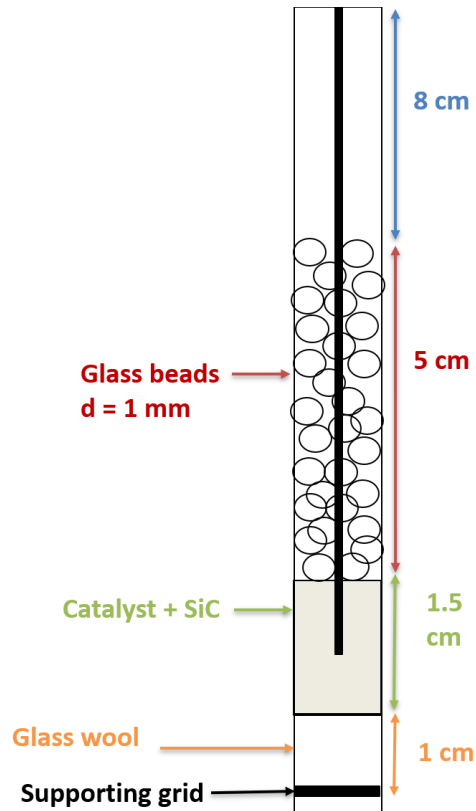
Catalyst testing

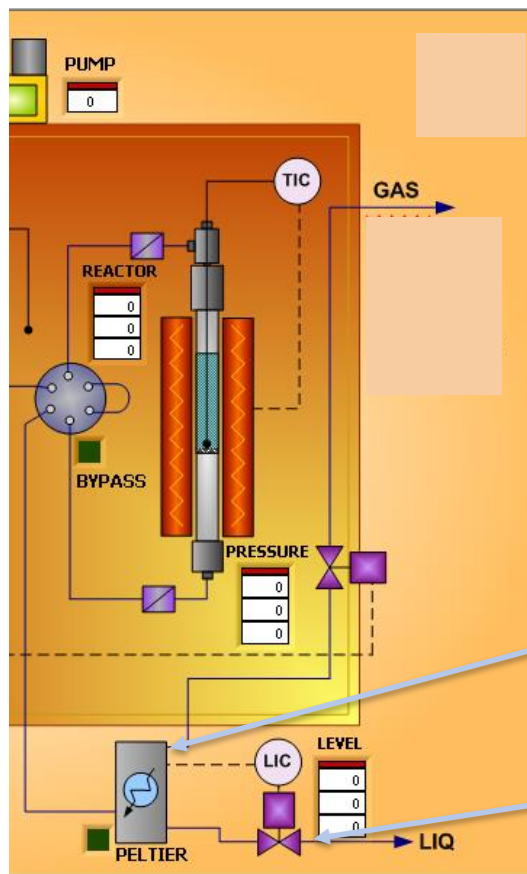


Catalyst testing



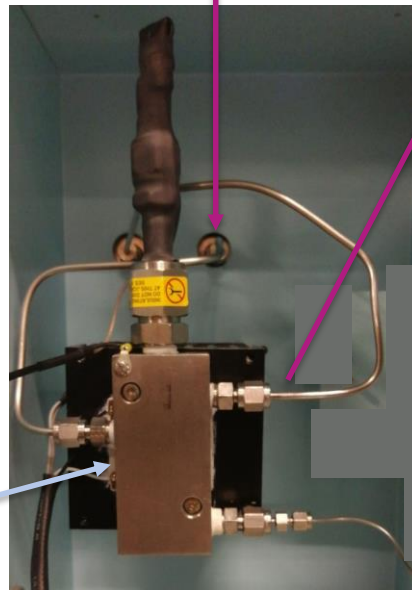
Catalyst testing





Products mixture from reactor

Gas products



Liquid products

Catalyst testing



	Conversion		Selectivity		TOF	r	TOS	N ₂ O-chemisorption		BET		
	end	loss	start	end	end	end	end	dispersion	d _{p,Cu}	S _{A,cat}	V _{pore}	d _{pore}
					[1/h]	[mol/(h*g _{cat})]	[h]	[%]	[nm]	[m ² /g]	[cm ³ /g]	[nm]
SNW	23%	30%	98%	97%	74.8	3.0E-03	49.5	5.0	11.6	570.2	0.8	5.5
SNE	24%	25%	97%	94%	85.9	3.3E-03	44	4.8	11.9	534.5	0.8	5.4
SNI	25%	36%	96%	95%	119.9	3.7E-03	49	3.9	14.7	529.2	0.8	5.8
SAW	30%	30%	96%	96%	128.6	3.9E-03	49	3.8	15.1	550.7	0.8	5.8
SAE	9%	28%	95%	95%	62.5	1.5E-03	49			585.0	0.9	6.8
SAI^a	5%	0%	72%	90%		5.7E-04	47			580.5	0.8	5.7
SCW	1%	34%	41%	0%	2.8	9.3E-05	49	4.2	13.6	561.6	0.7	5.2
SCE	1%	0%	17%	39%	4.8	1.8E-04	49			523.8	0.7	5.7
CNW	17%	3%	95%	94%	27.0	2.0E-03	46	9.5	6.0	81.5	0.3	13.1
CNE^b	11%	23%	92%	92%	8.3	1.4E-03	47	22.2	2.6	95.2	0.1	5.1
CNI	17%	0%	93%	94%	31.5	2.1E-03	46	8.4	6.8	96.0	0.1	5.1
CNI_at700^a	31%	39%	94%	96%		3.6E-03	47					
CNI_at1000	27%	40%	96%	97%		3.0E-03	47					
CCW	1%	0%	48%	17%	3.4	1.5E-04	49	5.5	10.5	95.2	0.1	5.0
CCE	0%	35%	0%	0%		8.8E-05	49			89.4	0.1	5.0

1st letter = S/C = SiO₂ / CNF

2nd letter = N/A/C = nitrate/acetate/carbonate

3rd letter = W/E/I = water/ethanol/isopropanol

Experiments performed at 240°C, 6bar (442mbar acetol, 3.4bar H₂) for 48h

^a 6 bar (355mbar acetol, 3.3 bar H₂)

^b 7bar (515 mbar acetol, 4 bar H₂)

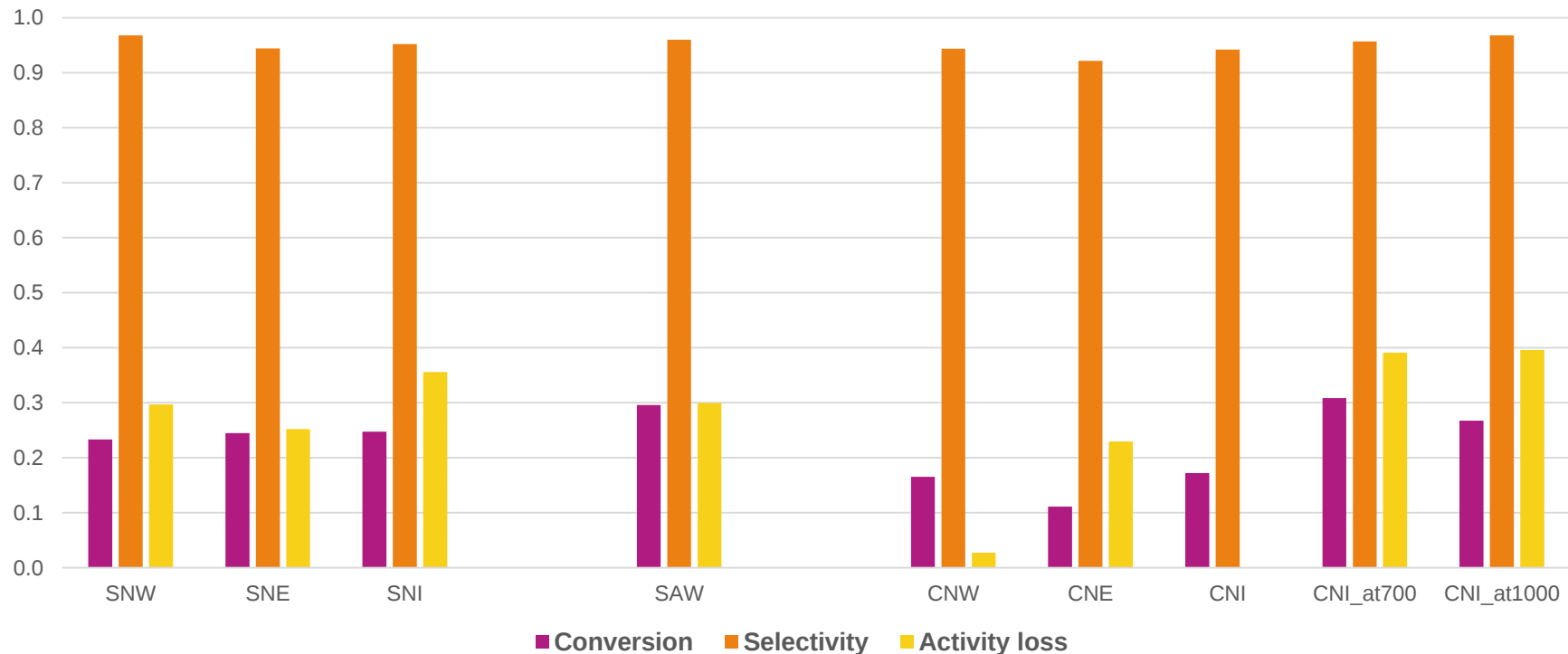
	Conversion		Selectivity		TOF	r	TOS	N ₂ O-chemisorption		BET		
	end	loss	start	end	end	end	end	dispersion	d _{p,Cu}	S _{A,cat}	V _{pore}	d _{pore}
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SNW	23%	30%	98%	97%	74.8	3.0E-03	49.5	5.0	11.6	570.2	0.8	5.5
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SNI	25%	36%	96%	95%	119.9	3.7E-03	49	3.9	14.7	529.2	0.8	5.8
SAW	30%	30%	96%	96%	128.6	3.9E-03	49	3.8	15.1	550.7	0.8	5.8
SAE	9%	28%	95%	95%	62.5	1.5E-03	49			585.0	0.9	6.8
SAI^a	5%	0%	72%	90%		5.7E-04	47			580.5	0.8	5.7
SCW	1%	34%	41%	0%	2.8	9.3E-05	49	4.2	13.6	561.6	0.7	5.2
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CNE^b	11%	23%	92%	92%	8.3	1.4E-03	47	22.2	2.6	95.2	0.1	5.1
CNI	17%	0%	93%	94%	31.5	2.1E-03	46	8.4	6.8	96.0	0.1	5.1
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CNI_at1000	27%	40%	96%	97%		3.0E-03	47					
CCW	1%	0%	48%	17%	3.4	1.5E-04	49	5.5	10.5	95.2	0.1	5.0
CCE	0%	35%	0%	0%		8.8E-05	49			89.4	0.1	5.0

1st letter = S/C = SiO₂ / CNF
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Experiments performed at 240°C, 6bar (442mbar acetol, 3.4bar H₂) for 48h
^a 6 bar (355mbar acetol, 3.3 bar H₂)
^b 7bar (515 mbar acetol, 4 bar H₂)

Catalysts screening

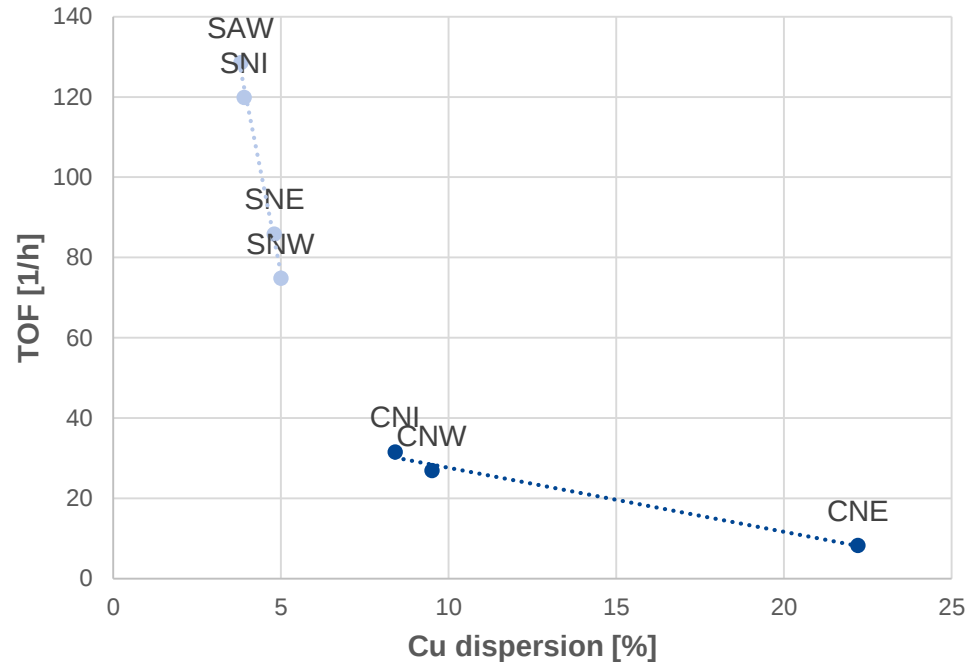
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Catalysts screening

Activity vs. dispersion

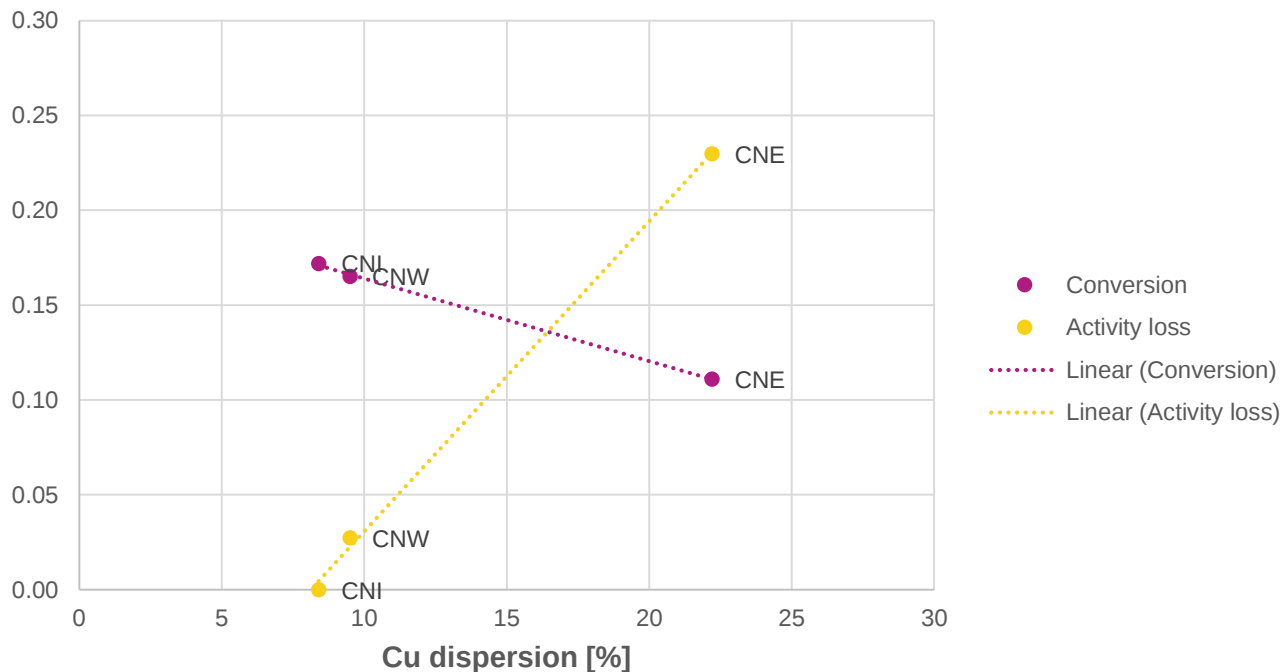
1st letter = S/C = SiO₂ / CNF
2nd letter = N/A/C = nitrate/acetate/carbonate
3rd letter = W/E/I = water/ethanol/isopropanol



Catalysts screening

Activity and activity loss

1st letter = S/C = SiO₂ / CNF
2nd letter = N/A/C = nitrate/acetate/carbonate
3rd letter = W/E/I = water/ethanol/isopropanol



Highlights of WP2.4 Catalysis



New Cu catalyst developed

Active, high selectivity (>95%)

Stable: no deactivation observed within 50 h



- ✓ Fundamental understanding of Cu catalysts in terms of particle size and support effects on the reaction
- ✓ Kinetic model of acetol hydrogenation

Future work

Preparation

Catalysts with higher Cu loading (15wt%)

Characterization

Complete properties study

Testing

- Selectivity study at higher conversion levels
- DMO hydrogenation

Writing

Publications and PhD thesis

Thank you!